

**AMENDMENTS TO THE SPECIFICATION**

**Please replace the second paragraph on page 1 with the following amended paragraph:**

The present invention relates to a process for producing polyorganosiloxane-containing resin, polyorganosiloxane-containing resin obtained by the process, and a ~~flameretardant flame-~~  
retardant comprising the polyorganosiloxane-containing resin.

**Please replace the first complete paragraph on page 2 with the following amended paragraph:**

In consideration of the environment and the ~~safety~~safety, from the viewpoint of handling properties represented by viscosity and heat transfer efficiency, polyorganosiloxane-containing resin which can be produced, stored and handled in the form of a dispersion in an aqueous medium is highly desired thus forming a big market.

**Please replace the first complete paragraph on page 14 with the following amended paragraph:**

Heating of the slurry in the apparatus and maintenance of the temperature of the slurry can be carried out by a method of heating an external jacket of the apparatus, a method of heating with a closed steam coil arranged in the apparatus, a method of introducing water vapor directly into the slurry, or a combination thereof. Introduction of water vapor is preferable because higher efficiency of vaporization of volatile siloxane can be achieved, and using a steam spray having suitably arranged pores, water vapor is preferably supplied through many pores into

the slurry, or water vapor is supplied from a considerably deep place under the liquid surface of the slurry, preferably from the bottom of the batch distillation apparatus.

**Please replace the paragraph bridging pages 20 and 21 with the following amended paragraph:**

The present invention also discloses polyorganosiloxane-containing resin whose volatile siloxane is reduced by heat-stripping the polyorganosiloxane-containing resin in a slurry state as described above. When the polyorganosiloxane-containing resin is made of a polyorganosiloxane-containing graft copolymer, heat stripping is conducted after conversion of polyorganosiloxane particles into slurry after all chemical reactions such as graft modification are concluded in the process of the present invention, and therefore, as compared with heat stripping of polyorganosiloxane particles in an emulsion state before graft modification, graft sites derived from a graft modifying agent can be utilized effectively in graft polymerization without undergoing change in a quality ~~quality~~ by heating.

**Please replace the last paragraph on page 24 with the following amended paragraph:**

Calculated as  $(\text{total amount of materials charged } (\text{parts}) \times \text{solids } (\text{parts}) \times \text{solids content} - (\text{amount of emulsifier charged } (\text{parts}) + \text{amount of inorganic acid and/or organic acid charged } (\text{parts}) + \text{amount of radical polymerization initiator } (\text{parts}) + \text{reducing agent } (\text{parts}) + \text{redox catalyst } (\text{parts}))) \times 100 / ((\text{parts}))) \times 100 / (\text{amount of monomers charged } (\text{parts})).$

**Please replace the first paragraph on page 25 with the following amended**

**paragraph:**

[Volume-average particle diameter]

The volume-average particle diameters of a seed polymer, polyorganosiloxane particles and a graft copolymer were measured respectively in a latex state ~~(元に戻しました)~~. Using a measuring instrument MICROTRAC UPA 150 manufactured by Nikkiso Co., Ltd., the volume-average particle diameter ( $\mu\text{m}$ ) was measured by a light scattering method.

**Please replace the paragraph bridging pages 29 and 30 with the following amended**

**paragraph:**

Then 0.05 part by weight of an ethylene oxide (22% content)-propylene oxide block copolymer (trade name: Pronone 102 manufactured by Nippon Oil & Fats Co., Ltd.) was added to 100 parts (in terms of solids content) by weight of the latex as an anti-foaming agent. Water vapor was fed at a rate of 3 kg/hour, and when the temperature was reached to 140°C, stripping was initiated. While the amount of distillate gas was controlled so as to maintain the temperature of the solution at 140 to 150°C, stripping was conducted for 30 minutes to give latices ~~give-latices~~-containing polyorganosiloxane particles (S-3, S-4) respectively.

**Please replace the paragraph bridging pages 39 and 40 with the following amended**

**paragraph:**

As can be seen from the above results, the volatile siloxane contained in the dehydrated cake of the polyorganosiloxane-containing resin obtained by the process of the present invention is reduced. It was also revealed that the water content of the dehydrated cake is reduced. That

is, this means that dissipation of volatile siloxane and load for drying are reduced in a subsequent drying ~~process~~process. Further, it can also be seen that volatile siloxane can be recovered well by the method of separating volatile siloxane from distillate components in the present invention.